## How to Establish a Bioregenerative Life Support System for Long-Term Crewed Missions to the Moon or Mars

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### Abstract

To conduct crewed simulation experiments of bioregenerative life support systems on the ground is a critical step for human life support in deep-space exploration. An artificial closed ecosystem named Lunar Palace 1 was built through integrating efficient higher plant cultivation, animal protein production, urine nitrogen recycling, and bioconversion of solid waste. Subsequently, a 105-day, multicrew, closed integrative bioregenerative life support systems experiment in Lunar Palace 1 was carried out from February through May 2014. The results show that environmental conditions as well as the gas balance between  $O_2$  and  $CO_2$  in the system were well maintained during the 105-day experiment. A total of 21 plant species in this system kept a harmonious coexistent relationship, and 20.5% nitrogen recovery from urine, 41% solid waste degradation, and a small amount of insect in situ production were achieved. During the 105-day experiment, oxygen and water were recycled, and 55% of the food was regenerated. Key Words: Bioregenerative life support systems (BLSS)—Space agriculture—Space life support—Waste recycle—Water recycle. Astrobiology 16, 925–936.

## 1. Introduction

♥ URRENT STRATEGIES to further explore space, such as ✓ NASA's Design Reference Architecture or China's lunar exploration program (Zheng et al., 2008; Drake et al., 2010), strongly suggest the development of bioregenerative life support systems (BLSS) that can be fully incorporated into space stations, transit vehicles, and eventually habitats on the Moon and Mars (Dempster et al., 2004; Tong et al., 2011). Utilization of BLSS would decrease resupply mass by regenerating essential resources for human use through biological processes. Within BLSS, the cultivation of higher plants takes a crucial role, as they can contribute to all major functional aspects (e.g., food production, carbon dioxide reduction, oxygen production, water recycling, and waste management) (Wheeler et al., 1993; Tikhomirov et al., 2003). The ultimate goal of this technology is to create a sustainable life support ecological environment that is open with respect to energy but closed with respect to mass (Massa et al., 2007). Technological innovation of BLSS unit components for biomass production and waste recycling is of particular interest for a number of researchers from various countries, including the United States, Russia, Japan, Canada, Germany, and China. Recent advances in unit technologies, particularly in the development of highefficiency plant cultivation (Fu et al., 2013; Dong et al., 2014c), animal protein production (Yu et al., 2008b; Li et al., 2016), nitrogen recovery from urine (Kabdasli et al., 2006), and bioconversion of solid wastes into soil-like substrate (Yu et al., 2008a; He et al., 2010; Tikhomirov et al., 2011), provide unparalleled opportunities to improve the closure coefficient of BLSS for the reduction of stowage, the resupply of life support materials, and the provision of more reasonable and balanced diets for crews.

As a simple model, BLSS address the interactions among organisms and their environment as an integrated system through the study of factors that regulate the pools and fluxes of materials and energy through the ecosystem. The flow of energy and materials through organisms and the physical environment provides a framework for understanding the diversity of form and functioning of Earth's physical and biological processes. The unique contribution of BLSS is their focus on biotic and abiotic factors as interacting components of a single integrated system.

Despite progress in the technology of BLSS unit components, the development of feasible bioregenerative systems

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requires the integration of these units into a single system. Russian (BIOS-3, 3–6 months) (Gitelson *et al.*, 1989; Salisbury *et al.*, 1997) and Japanese investigators (CEEF, 1–4 weeks) (Tako *et al.*, 2008, 2011) have conducted crewed simulation experiments by integrating several BLSS unit components on the ground. These studies demonstrate that the different biological components and operational methods result in changes of mass circulation and migration in BLSS (Nelson *et al.*, 2009; Tong *et al.*, 2012).The information on BLSS mass flow integrated with currently available new unit technologies, as mentioned above, is therefore needed to establish realistic BLSS in the future.

In the present study, we established a ground-based experimental BLSS platform (Lunar Palace 1) by integrating atmospheric management, crop production, insect breeding, waste recovery, and water-processing compartments. With this system, we performed a 105-day, multicrew, closed integrative experiment wherein several new technologies for BLSS that comprise high-efficiency plant cultivation, animal protein production, urine nitrogen recycling, and bioconversion of solid wastes into soil-like substrate were applied. The mass flow of the system was analyzed and compared with other published reports. Moreover, we also explored the quantitative relationships of material flux among different components of the system. Efforts like Lunar Palace 1 will yield important information in preparation for missions to the Moon or Mars.

#### 2. Materials and Methods

#### 2.1. Sealed research facility

The integrative, ground-based, experimental facility for Permanent Astrobase Life-support Artificial Closed Ecosystem (P.A.L.A.C.E.) was rigorously designed according to the definition of BLSS and is referred to as Lunar Palace 1. Lunar Palace 1 comprises a comprehensive cabin and two plant cultivation cabins. Its construction was divided into two stages. The first stage included construction of a  $14 \times 3 \times 2.5$  m comprehensive cabin and a  $10 \times 5.8 \times 3.5$  m plant cabin, which have the capacity to provide three crew members with a life support environment. In the second stage, another plant cabin will be built, with a capacity for five members to live. The present study was conducted by using the Lunar Palace 1 first-stage facility. The comprehensive cabin included four private bedrooms, a living room, a bathroom, and a room for waste treatment. The plant cultivation cabin was subdivided into two rooms, that is, plantculture room 1 and 2. The environmental conditions within these two plant rooms were controlled separately, according to the growth demands of different plants. To provide a hermetic environment, the facility's shell was welded stainless steel plates, and all cabin doors were tightly sealed with silicon gaskets. We used far higher CO<sub>2</sub> concentration changes to test the leakage rate of the closed system (Dempster et al., 2009; Tong et al., 2011), and a leakage rate of 0.04% per day was obtained (Dong et al., 2016a).

### 2.2. Key modules

New unit technologies, including nitrogen recovery from urine, soil-like substrate preparation by co-fermentation of straw and human feces, and animal protein production using plant wastes were integrated into Lunar Palace 1. In terms of function, Lunar Palace 1 was divided into three key modules: a higher plant cultivation module, a water treatment module, and a solid waste bioconversion and animal-rearing module.

#### 2.3. Higher plant cultivation module

A spatial multilayer planting method was employed in the plant cultivation module to improve space-utilization efficiency of the plant cabin (Dong et al., 2015b). The plant cultivation module was composed of 13 three-layer plant trays, where five food crops, 15 vegetables, and one fruit were cultivated (Dong et al., 2016b). The total growing area for crops was  $69 \,\mathrm{m}^2$ . Here, the plant species and abundance were designed based on a set of criteria of human nutritional requirements and dietary variety (Yang et al., 2002; Hu et al., 2010). The cultivation schedule for all varieties of plants is shown in Supplementary Table S1 (Supplementary Data are available online at www.liebertonline.com/ast). A variety of plants were introduced into the system as seeds and conveyortype cultivated with uniform and sustained oxygen production. A red-white light-emitting diode (LED) with full light spectra arrays was used as a light source for plant growth (Dong et al., 2014a). The illumination conditions were set as follows: in room 1, continuous lighting was provided, with a light intensity of  $500 \,\mu\text{mol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$  (as tested from 20 cm below the light source) (Dong *et al.*, 2014b); in room 2, a  $16 \,\text{h}\cdot\text{d}^{-1}$ lighting period (light:dark=16:8 h) was employed with the same light intensity as room 1. All plants were irrigated regularly with 1 or 2 a time-strength modified Hoagland solution (Dong et al., 2015a), and the pH was kept at 5.8-6.0. Modified Hoagland solution was prepared by stored plant minerals that were supplied into the system periodically.

### 2.4. Water treatment module

This module was subdivided into three units, that is, a humidity condensate water processing unit, a sanitary wastewater treatment unit, and a urine treatment unit. The water processing procedures of the system are shown in Fig. 1. With air cooling facilities, plant transpiration of the plant cabin produced a large amount of humidity condensate water. The condensed water from the plant cabin and the comprehensive cabin was collected and pumped through water purification equipment. The purified water was then stored in a clean water tank. Most of the purified water was used for plant nutrient solution preparation, and the rest served as drinking water and sanitary water for the crew. The urine collected from the crew was treated with low-pressure distillation to recover water and part of the nitrogen. The recovered water was mixed with sanitary wastewater from the comprehensive cabin before going through a biological activated carbon membrane reactor for purification. The purified water was then collected into a gray-water tank before being pumped into the nutrition tank for the preparation of plant nutrient solution. The solid residual urine obtained from distillation was collected, stored, and periodically sent out of the system.

### 2.5. Solid waste bioconversion and animal-rearing module

The inedible crop biomass (mainly stalks) was dried and ground into powder after the plants were harvested. A total



FIG. 1. Water recovery procedures during the 105-day experiment in Lunar Palace 1.

of 85.8% of the straw powder was stored for fermentation, 13.9% as bedding for human feces, and 0.3% for insect (yellow mealworm, Tenebrio molitor L.) food fermentation, along with some old vegetable leaves produced in the system. The stored straw powder, the human feces with straw bedding, and worm frass were sent collectively into a solid waste bioconverter that contained microbial inoculants that are able to degrade plant waste. The CO<sub>2</sub>-enriched gas released from the solid waste bioconverter was passed through an air purifier and into the plant cabin to supply CO<sub>2</sub> for plant photosynthesis. Moreover, to control and limit CO<sub>2</sub> fluctuation, the  $CO_2$  emission rate from the bioconverter to the plant cabin was regulated by controlling the amount of running heat units inside the bioconverter based on a feedback signal of CO<sub>2</sub> concentration. Compressed solid residues that remained after fermentation were stored and periodically exported from the system. The technological process of solid waste treatment is shown in Fig. 2.

### 2.6. Crew and substitutions

To test the toleration capacity of Lunar Palace 1 for crew members, a total of five volunteers was selected and trained to participate in a 105-day closed test experiment. The basic physical information gathered from these volunteers is listed in Table 1. The volunteers maintained good health and good psychological compatibilities and were devoid of habits detrimental to their overall health (*e.g.*, smoking, drinking alcohol). The 105-day experiment was performed from February 3 to May 20, 2014. The study was approved by the Committee of the School of Biological Science and Medical Engineering in Beihang University, Beijing, China (Approval ID: 20140203, approval date January 15, 2014). This study was carried out in strict accordance and compliance with the Statement on Ethical Conduct in Research Involving Humans guidelines of the Science and Medical Engineering in Beihang University. Written informed consent was obtained from all volunteers.

## 2.7. Environmental monitoring and control of the system

Within the entire closed experiment, environmental parameters that included cabin temperature, humidity, air pressure, and air composition ( $O_2$  and  $CO_2$  concentrations) were monitored continuously by a series of sensors located at a variety of positions within the system (Fig. 3). Accordingly, cabin temperature and humidity were controlled in real-time by airconditioners and dehumidifiers. Furthermore, levels for 14 kinds of harmful trace gases were determined weekly with gas chromatography–mass spectrometry, using the EPA TO-14



FIG. 2. Solid waste processing procedures during the 105-day experiment in Lunar Palace 1.

method (EPA/625-96/010b). Seven representative air sampling points were selected in the plant chamber and comprehensive chamber. For crew and plant safety, air purification devices were installed in system ventilation pipes for removing harmful gases. The air purification devices were composed of an electrostatic precipitator, an activated charcoal matrix, and a catalytic reactor, and were run continuously for  $24 \text{ h} \cdot \text{d}^{-1}$  without maintenance during the entire experimental period.

## 2.8. Dynamic monitoring and balance control in gas and water

By distributing the sensors at multiple points within the system, dynamic changes in  $CO_2$  and  $O_2$  concentrations were monitored and recorded in real-time. When the con-

 TABLE 1. BASIC INFORMATION ON THE CREW

 MEMBERS IN THE 105-DAY EXPERIMENT

Crew member	Gender	Age (yr)	Body weight (kg)	Body height (cm)
A	Male	28	75	180
В	Male	25	70	175
С	Male	33	85	183
D	Female	30	47	160
E	Female	32	42	153

centration of internal CO<sub>2</sub> exceeded 5000 ppm (*i.e.*,  $\mu$ mol/mol), the concentrations of O<sub>2</sub> and CO<sub>2</sub> were regulated by adjusting the solid waste bioconverter temperature, the lighting period of plants, and the intensity of crew activities. With respect to the water, no extra water was imported into the system during the experiment. The water consumption by the crew and plant irrigation, as well as water recovered from air condensation, urine, and sanitary wastewater, were monitored and recorded.

## 2.9. Biomass and waste measurements

The edible biomass, inedible biomass, and nutritional elements of the crops were measured after harvesting each batch of crops. The  $O_2$  production efficiencies were calculated with stoichiometric models (Tikhomirov *et al.*, 2003; Hu and Bartsev, 2010). Urine and feces from the crew and worm frass were collected and weighed. The  $O_2$  consumption and  $CO_2$  production rates during the process of solid waste treatment were calculated by testing the element composition of each material and building stoichiometric models (Hu *et al.*, 2010).

## 2.10. Crew basal metabolic rate measurements and external food supplements

During the entire experiment, the total energy expenditure (TEE) of each crew member was recorded through an



FIG. 3. Distribution of different sensors, locations, points in Lunar Palace 1.

energy consumption meter and expressed by using the Weir equation (Weir, 1949):

$$\text{TEE} = 3.941 \times r\text{O}_2 + 1.106 \times r\text{CO}_2 - 2.17 \times \text{UN} \quad (1)$$

where UN is the nitrogen in urine  $(g \cdot d^{-1})$ ,  $rO_2$  is the consumption of  $O_2$  (L·min<sup>-1</sup>), and  $rCO_2$  is the exhalation of  $CO_2$  (L·min<sup>-1</sup>). The unit of TEE is kilocalories per day (kcal·d<sup>-1</sup>).

The respiratory quotient (RQ), which is defined as  $rCO_2/rO_2$ , was calculated according to the crew's metabolism (Livingstone *et al.*, 1990).

Thus, the daily  $O_2$  consumption and  $CO_2$  exhalation were obtained. Combined with the yield and nutrition of different crops and TEE of the crew, the daily diet composition of the crew and the quantity of external food supply were determined. External food such as meat was supplied into the system periodically.

# 2.11. The calculation of regeneration efficiency and closure coefficient of BLSS

The calculation formula of oxygen, water, and food regeneration efficiency (R) was as follows:

$$R = \left(1 - \frac{\mathrm{mi}}{\mathrm{Mi}}\right) \times 100\% \tag{2}$$

where mi is the amount of daily oxygen, water, or food supplied from outside (g); Mi is the amount of daily oxygen, water, or food consumption by the crew (g).

The closure coefficient (C) of the bioregenerative lifesupport system was calculated by the following equation (Gitelson and Lisovsky, 2003):

$$C = \left(1 - \frac{m}{M}\right) \times 100\% \tag{3}$$

## 3. Results

# 3.1. Atmospheric environment control during 105-day closed experiment

The air temperature and humidity of the comprehensive cabin and plant-culture rooms were stable over the 105-day experiment (Fig. 4A). Both temperature and humidity correspond to the standard of plant growth and human habitation in advanced life support systems (Hanford, 2006). We next determined the concentrations of 12 different harmful trace gases for both Pre-Test (from day –15 to day 0) and Test periods (from day 0 to day 105) to analyze air quality of the closed environment. The concentrations of ammonia, carbon monoxide, formaldehyde, hydrogen sulfide, toluene, ethylbenzene, acrolein, ethanol, ozone, methane, sulfur dioxide, and nitrogen dioxide did not exceed the spacecraft maximum allowable concentration (SMAC) (James, 2008) in either case (Fig. 4B). Furthermore, the concentrations of

nitrogen oxides  $(NO_x)$  and total volatile organic compounds (TVOC) were also far lower than the SMAC.

The  $O_2$  concentration in Lunar Palace 1 was maintained within the range of 19.5–21.5%, while the  $CO_2$  concentration was controlled between 500 and 5500 ppm (Fig. 4C). The variation of gas could be divided into two stages. The first stage was the first 26 days, when  $O_2$  and  $CO_2$  concentrations fluctuated greatly with crew substitutions (Fig. 5). We could clearly see that  $CO_2$  concentration rapidly increased from 900 to 5500 ppm from day 8 to day 11, when three male volunteers (A, B, and C) were confined. The second stage was from day 26 to day 105, when one male (A) and two females (D and E) were combined; fluctuation range of  $O_2$  and  $CO_2$  concentrations gradually narrowed with increasing time of closure and achieved a relative steadystate level at the end of the experiment.

### 3.2. Water recovery

The data of daily water consumption and regeneration of the crew members A, D, and E are shown in Table 2. From these results, we found that 100% of water regeneration was achieved. The tiny difference between the daily water



**FIG. 4.** (A) Temperature and humidity in comprehensive cabin (i), plant-culture room 1 (ii), and plant-culture room 2 (iii); (B) the concentration changes of trace harmful gases (i and ii); and (C)  $CO_2$  and  $O_2$  fluctuations during the whole closed experimental period.



FIG. 5. Crew substitutions during the 105-day experiment in Lunar Palace 1.

consumption (317.04 L) and regeneration (316.75 L) might be due to a statistical error. Therefore, the water pre-stored in the system was used and recycled continuously during the whole process of the 105-day experiment, and no extra water needed to be supplied from outside.

## 3.3. Food production and efficiency of O<sub>2</sub> production

Tables 3 and 4 show the production efficiencies of edible biomass and  $O_2$  production ability of the crops during the 105-day closed experiment, respectively. For Lunar Palace 1, wheat was used as the main food crop and was thereby the major producer of  $O_2$ . Its  $O_2$  production ability was  $33.32 \text{ g} \cdot \text{m}^{-2} \cdot \text{d}^{-1}$  (Table 4). The  $O_2$  production ability of leafy vegetables was the lowest, with an average value of  $7.23 \text{ g} \cdot \text{m}^{-2} \cdot \text{d}^{-1}$ . Even so, it was still necessary to cultivate a certain area of leafy vegetables for matching between food supply and human nutritional requirements in the closed environment (Tako *et al.*, 2011).

## 3.4. Crew metabolism and waste treatment

The average daily food consumption of the crew members A, D, and E was 1431 g per day, which is equal to 5900 kcal of energy, with 15% content for protein, 28% for fat, and 57% for carbohydrate (Fig. 6A-ii). The TEE evaluated by the accelerometer showed that the average daily energy expenditure for the male crew member A was 2600 kcal, and between 1600 and 1700 kcal for each of the two female members D and E (Fig. 6A-i). The sum of daily energy consumption of the three crew members approximately equaled their daily food energy intake in theory. However, a decrease of less than 2 kg in body weight of each crew member was observed when comparing the data before and after the closed experiment. This might be caused by many factors such as psychological factors, food-utilizing efficiency, and water consumption, and the issue needs to be further investigated. The average daily urine and feces produced by three

		× ,		
Water consumption		Water recovery		
Crew		Condensate water	270.4	
Potable water	2.97			
Water for food preparation	10.23	Water recovered from urine	3.01	
Water for dishware cleaning	6.11			
Water for cabin cleaning	4.84	Water recovered from sanitary wastewater	43.34	
Water for facial cleaning	7.3	•		
Water for feet washing	6.47			
Laundry water	4.97			
Bath water	4.35			
Plants				
Plant irrigation water	269.8			
Total	317.04		316.75	

TABLE 2. WATER CONSUMPTION AND RECOVERY DURING THE 105-DAY EXPERIMENT UNDER THE THREE-CREW-MEMBER MODE  $(KG \cdot D^{-1})$ 

gation (Fig. 6C-i). For solid waste treatment, 15,994 g (dry

weight) of straw powder, 281 g (dry weight) of worm frass, and 17,566 g (dry weight) of human feces were added to the solid waste bioconverter (Fig. 6C-ii). After 105 days, a total of 21,760 g solid waste residue was discharged. Therefore, the degradation efficiency of solid waste reached 41.0%, and the average degradation rate of dry

Stoichiometric models are widely used in assessing material fluxes under the balanced condition of the system. To simplify the calculation and gain more precise analysis, we

chose four major elements, C, H, O, N, to perform the stoichiometry calculations. The molecular formula of each

material was obtained through elemental analysis or by

previous research (Tikhomirov et al., 2003; Hu et al., 2010).

Consequently, the stoichiometric models for plant growth,

crew metabolism, solid waste treatment, and animal rearing

3.5. System mass flow and closure coefficient

Crop	Lunar Palace 1 (dry weight, $g \cdot m^{-2} \cdot d^{-1}$ )
Wheat	12.81±2.27*
Chufa	$8.31 \pm 1.32$
Soybean	$5.31 \pm 1.75$
Kidney bean	$10.18 \pm 1.36$
Leafy vegetables	$5.99 \pm 0.56$
Carrot	$3.58 \pm 0.21$
Cucumber	$10.03 \pm 1.46$
Green onion	$33.88 \pm 2.47$
Strawberry	$3.25 \pm 0.22$

TABLE 3. CROP PRODUCTION EFFICIENCY OF EDIBLE BIOMASS DURING THE 105-DAY EXPERIMENT

\*Mean  $\pm$  SE.

members were 3295 mL and 658 g (fresh weight), respectively (Fig. 6B-i, 6B-ii).

During the entire closed experiment, the total urine processed by the crew was 346 L, from which 100% of water and 20.5% of nitrogen was recycled for plant irri-

Plant growth

$$58.04503 \text{ CO}_{2} + 46.24993 \text{ H}_{2}\text{O} + 0.77729 \text{ NH}_{3} + 2.06166 \text{ HNO}_{3} \longrightarrow 0.11356 \text{ C}_{100}\text{H}_{159}\text{O}_{31}\text{N}_{25} + 0.11358 \text{ C}_{57}\text{H}_{104}\text{O}_{6} + 6.70250 \text{ C}_{6}\text{H}_{10}\text{O}_{5} + 65.40535 \text{ O}_{2} \tag{4}$$

were identified as follows:

matter was  $141 \text{ g} \cdot \text{d}^{-1}$ .

Human metabolism

$$\begin{array}{l} 0.11559 \ C_{100}H_{159}O_{31}N_{25} + 0.23556 C_{57}H_{104}O_6 + 6.00674 C_6H_{10}O_5 + 60.10082 \ O_2 \longrightarrow \\ 53.28713 \ CO_2 + 43.51308 \ H_2O + 0.01713 C_{100}H_{331}O_{86}N_{151} \\ + 2.06166 C_{100}H_{170}O_{61}N_5 + 0.00021 C_{100}H_{190}O_{40}N_{16} \\ & \text{body waste} \end{array}$$

$$(5)$$

Solid waste treatment

$$0.01829 C_{308} H_{397} O_{340} N_{18} + 0.06919 C_{100} H_{170} O_{61} N_5 + 0.25435 HNO_3 + 5.30021 O_2$$
  
straw and worm frass  

$$----- 4.70361 CO_2 + 5.61485 H_2O + 0.02105 C_{373} H_{627} O_{286} N_{21} + 0.25435 NH_4 NO_3 N_5$$
(6)

Animal rearing

$$\begin{cases} 0.00052 C_{100}H_{159}O_{31}N_{25} + 0.00043 C_{57}H_{104}O_6 + 0.01216 C_6H_{10}O_5 \\ \text{sugar} \\ + 0.01877 C_6H_{10}O_5 + 0.00053 C_{10}H_{11}O_2 \\ \text{fiber} \\ + 0.05392 O_2 \longrightarrow 0.04652 CO_2 + 0.04021 H_2O \\ + \left\{ 0.00018 C_{100}H_{159}O_{31}N_{25} + 0.00007 C_{57}H_{104}O_6 + 0.00032 C_6H_{10}O_5 \\ \text{protein} \\ \text{fat} \\ + 0.010034 C_{100}H_{159}O_{31}N_{25} + 0.00004 C_{57}H_{104}O_6 + 0.01174 C_6H_{10}O_5 \\ \text{protein} \\ \text{fat} \\ + 0.01417 C_6H_{10}O_5 + 0.00053 C_{33}H_{38}O_{12} \\ \text{fiber} \\ \text{lignin} \\ \end{bmatrix}_{\text{frass}} \end{cases}$$
(7)

Crop	Total biomass (dry weight, $g \cdot m^{-2} \cdot d^{-1}$ )	Carbon content (%)	$CO_2 uptake$ $(g \cdot m^{-2} \cdot d^{-1})$	$O_2 \ production \ (g \cdot m^{-2} \cdot d^{-1})$
Wheat	33.36	39.68	45.81	33.32
Chufa	14.50	41.99	21.10	15.35
Soybean	17.76	41.14	27.34	19.88
Kidney bean	18.31	40.28	27.62	20.09
Leafy vegetables	6.73	31.14	9.94	7.23
Carrot	6.85	40.60	7.81	5.69
Cucumber	30.03	40.68	44.70	32.51
Green onion	35.66	43.01	53.20	38.69
Strawberry	12.31	39.68	19.38	14.09
Peanut	20.51	57.35	43.13	31.37
Corn	8.69	33.63	10.72	7.80

TABLE 4. ABILITIES OF PLANT CROPS IN LUNAR PALACE 1



**FIG. 6.** (A) Daily energy expenditure (i) and daily food intake and percent of total energy (ii) of three crew members; (B) average daily feces (i) and urine (ii) produced by three crew members; (C) performance of urine treatment (i) and solid waste treatment (ii) during the whole closed experiment.



**FIG. 7.** Mass flow relationships among system components  $(g \cdot d^{-1})$ . Arrows indicate the material flow direction. Object boxes represent each biological unit. Solid matter, liquid, and gas flows are marked by black, blue, and red arrows, respectively. Data of solid matter was on a dry-weight basis.

Based on the coefficients in Eqs. 4–7 and the quantity of water and food measured during the whole experiment, the mass flow relationships among solid materials, liquid, and gas in the system with an ideal stable state are illustrated graphically in Fig. 7. The O<sub>2</sub> production rate of the plant cabin was  $2093 \text{ g} \cdot \text{d}^{-1}$ , most of which was consumed by human respiration ( $1923 \text{ g} \cdot \text{d}^{-1}$  of O<sub>2</sub> consumption), though a small proportion was utilized in solid waste fermentation and animal rearing ( $170 \text{ g} \cdot \text{d}^{-1}$ ). To maintain mass balance,  $1256 \text{ g} \cdot \text{d}^{-1}$  of exogenous food and salts for crew and minerals for plants was supplied into the system, and the equivalent mass of solid waste residue, plant inedible biomass, and residual solid from urine was stored daily and periodically sent out of the system.

The materials consumed by crew members under the stable running status of Lunar Palace 1 are shown in

Table 5. Combined with Eqs. 2 and 3 (Gitelson and Lisovsky, 2003), we found that a regeneration rate of 100% was achieved for water and oxygen, and 55% for the food (61% of the plant food). The overall closure coefficient in Lunar Palace 1 was 97%.

#### 4. Discussion

These results demonstrate that the maximum capacity of CO<sub>2</sub> absorption with 69 m<sup>2</sup> of crops in Lunar Palace 1 was insufficient to meet the breathing requirements for three male crew members but greater than or equal to the requirement of one male and two females. This is in agreement with an earlier report from the Russian BIOS-3 project and NASA testing, which indicated that  $\sim 20-25$  m<sup>2</sup> of crops could only supply sufficient oxygen for one human (Yorio *et al.*, 2001).

TABLE 5. MATERIAL CONSUMPTION BY THE CREW COMPOSED OF 1 MALE AND 2 FEMALES

Material consumption by the	$crew (g \cdot d^{-1})$	Materials supplied from	$i \text{ outside } (g \cdot d^{-1})$
1. Food (dry weight)	1,254	1. Food (dry weight)	564
2. Salt	18	2. Salt	18
3. Oxygen	1,923	3. Plant nutrients	674
4. Potable water	2,970	4. Plant seeds	0.23
5. Water for food preparation	4,540	5. Toilet tissue	18
6. Sanitary water	39,040	6. Cleaning supplies	10.7
7. Toilet tissue	18		
8. Cleaning supplies	10.7		
Total	<i>M</i> =49,773.7		m = 1,284.93

In addition, the rapid rise of  $CO_2$  concentration from day 8 to day 11, once again, proved the good air-tightness of the system. Together, these data demonstrate that the atmospheric environment control in the system, including air-tightness, temperature, and relative humidity, as well as a reasonable fluctuation range of  $O_2$  and  $CO_2$ , was well achieved.

According to Table 2, we also concluded that household water consumption was  $47.24 \text{ kg} \cdot \text{d}^{-1}$ , that is, 15.77 kg per capita per day. This number was between the water demand of an early planetary base and a mature planetary base (Hanford, 2006). Additionally, plant transpiration rate averaged  $3.91 \text{ L} \cdot \text{m}^{-2} \cdot \text{d}^{-1}$ , which was similar to that of previous studies (Tako *et al.*, 2008; Wheeler *et al.*, 2008).

In general, the energy metabolism level of the crew in Lunar Palace 1 was similar to that of an early study in CEEF (Komatsubara *et al.*, 2005), but the daily energy intake was lower than the recommended values by Levine *et al.* (1996) (2900 kcal for the man and 2200 kcal for the woman). Interestingly, the daily fecal excretion by the crew in our study was far higher than daily mean fecal excretion of 110–170 g reported by Hanford (2006) and similar to the NASA STD-3000 (or 3001) (Gill and Vaughan, 2003). This could be attributed to the fact that vegetables accounted for the majority of the crew's food intake. A prior study by Hawk also showed that the daily mean fecal excretion for an individual on a vegetarian diet could be as much as 350 g (Oser, 1965).

Compared with the results of the Russian and Japanese systems, the food regeneration rate in Lunar Palace 1 was higher than in the BIOS-3 experiment that involved three crew members (48%) and was lower than in the BIOS-3 experiment with two crew members (78%) and was lower than in the Japanese system with two crew members (90%) (Gitelson and Lisovsky, 2003; Tako *et al.*, 2011). We believe that the differences in closure coefficient and food regeneration rate between our system and other systems were due to differences in system design and participants.

Bioregenerative life-support systems are complex networks of interacting feedbacks. The acquisition of water, nutrients, and light to support growth of one plant, for example, reduces availability of these resources to other plants, thereby constraining community productivity. The interactive controls both respond to and affect ecosystem processes. There are also positive feedbacks in BLSS in which both components of a system have a positive effect on the other or both have a negative effect on one another.

## 5. Conclusions

Lunar Palace 1 provides a simplified system that can be studied in great detail and offers insight into processes that occur at global scales in Earth's biosphere. Conversely, the global budgets of materials that cycle between the atmosphere, land, and oceans provide a context for understanding the broader significance of processes studied in a particular ecosystem. The essential biotic components of BLSS include plants that bring carbon and energy into the ecosystem, decomposers that break down dead organic matter and release  $CO_2$  and nutrients, and crew members who transfer energy and materials within the small ecosystem and operate technical systems that support and control the activity of plants and decomposers.

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### **Abbreviations Used**

BLSS = bioregenerative life-support systems SMAC = spacecraft maximum allowable

- concentration TEE = total energy expenditure
- TVOC = total volatile organic compounds